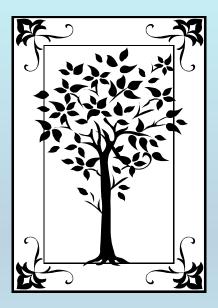
## METADATA AND NUMERICAL DATA CAPTURE: DENSITY (2 component mixture)

# Guided Data Capture (GDC)



This tutorial decribes METADATA AND NUMERICAL DATA CAPTURE: for **DENSITIES (2 components)** with the Guided Data Capture (GDC) software.

## NOTE:

The tutorials proceed sequentially to ease the descriptions. It is not necessary to enter *all* compounds before entering *all* samples, etc.

Compounds, samples, properties, etc., can be added or modified at any time.

However, the hierarchy must be maintained (i.e., a property cannot be entered, if there is no associated sample or compound.)

#### The experimental data used in this example is from:

J. Chem. Eng. Data 2002, 47, 811-815

#### 811

#### Density and Refractive Index at 298.15 K and Vapor–Liquid Equilibria at 101.3 kPa for Four Binary Systems of Methanol, *n*-Propanol, *n*-Butanol, or Isobutanol with *N*-Methylpiperazine

#### Shuda Chen,<sup>†</sup> Qunfang Lei, and Wenjun Fang\*

Department of Chemistry, Zhejiang University, Hangzhou 310027, Zhejiang, People's Republic of China

Density and refractive index data at 298.15 K, and isobaric vapor—liquid equilibrium (VLE) measurements at 101.3 kPa were reported for four binary systems of methanol, *n*-propanol, *n*-butanol, or isobutanol with *N*-methylpiperazine. Excess molar volumes and refractive index deviations were calculated. The measurement results exhibit no azeotropes for VLE, negative values for excess molar volume, and positive deviations from ideality for the refractive index over the whole mole fraction range. Liquid-phase activity coefficients and vapor-phase fugacity coefficients were estimated taking into account the nonideal nature of the vapor and liquid phases. The VLE data were shown to be thermodynamically consistent and were correlated by the UNIQUAC liquid-phase activity coefficient model with temperature-dependent parameters.

#### Densities (liquid phase) for **(methanol + N-methylpiperazine)** at T = 298.15 K and p = 101.3 kPa

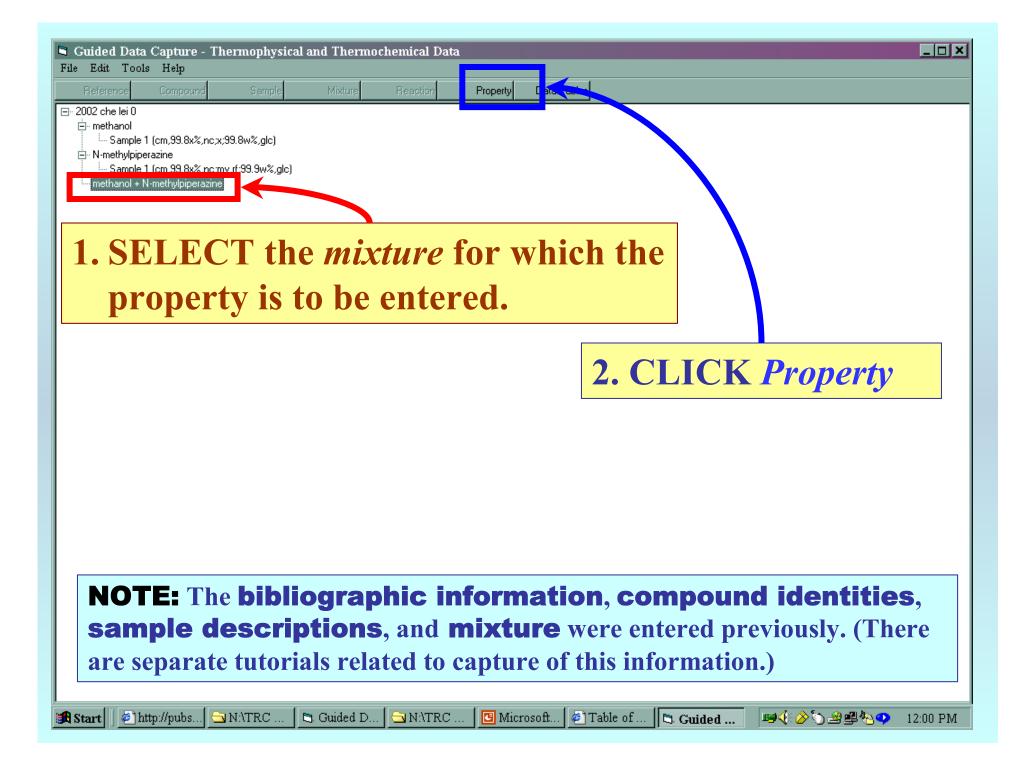
Table 3. Density  $\rho$  and Excess Molar Volume  $V^{E}$  for Binary Mixtures of Alkanol (1) + N-Methylpiperazine (2) at 298.15 K

	ρ	$V^{\mathbf{E}}$		ρ	$V^{E}$
$x_1$	$\rm g\cdot cm^{-3}$	$\mathrm{cm}^3\cdot\mathrm{mol}^{-1}$	XI	g•cm <sup>-3</sup>	$\text{cm}^3 \cdot \text{mol}^{-1}$
Metl	(1) +	NMP (2)	<i>n</i> -Pro	panol(1) +	NMP (2)
0.0498	0.89954	-0.225	0.0483	0.898.02	-0.187
0.1050	0.899.14	-0.463	0.1012	0.895~74	-0.361
0.1491	0.898~68	-0.641	0.1395	0.894.07	-0.492
0.2052	$0.897\ 88$	-0.848	0.1465	0.893~78	-0.519
0.2503	0.897~23	-1.020	0.1950	0.891.38	-0.661
0.2996	$0.896\ 17$	-1.178	0.2439	0.88898	-0.815
0.3488	0.894 96	-1.330	0.2936	0.88606	-0.930
0.3989	0.893 39	-1.465	0.3473	0.882~79	-1.056
0.4492	0.891.59	-1.593	0.3914	0.87995	-1.153
0.5006	$0.889\ 11$	-1.686	0.4476	0.875~98	-1.255
0.5618	0.885~69	-1.787	0.4913	0.872 65	-1.323
0.6001	0.882~75	-1.807	0.5452	0.868.03	-1.370
0.6497	0.87842	-1.822	0.5934	0.86355	-1.395
0.7052	0.872.25	-1.789	0.6424	0.858.59	-1.399
0.7521	$0.865\ 54$	-1.707	0.6922	0.853.04	-1.372
0.8001	$0.856\ 87$	-1.563	0.7420	0.846~78	-1.299
0.8490	0.84558	-1.340	0.7941	0.83947	-1.177
0.8978	0.83109	-1.023	0.8425	0.831~79	-1.006
0.9490	0.81144	-0.571	0.8954	0.822 30	-0.749
			0.9474	0.811.76	-0.419

#### **Experimental Method:**

Densities of all the samples were measured by using a <u>vibrating tube digital densimeter</u>, model DMA 602 (Anton Paar), thermostated with a circulating-water bath with a precision of  $\pm 0.01$  K. Refractive indices were determined

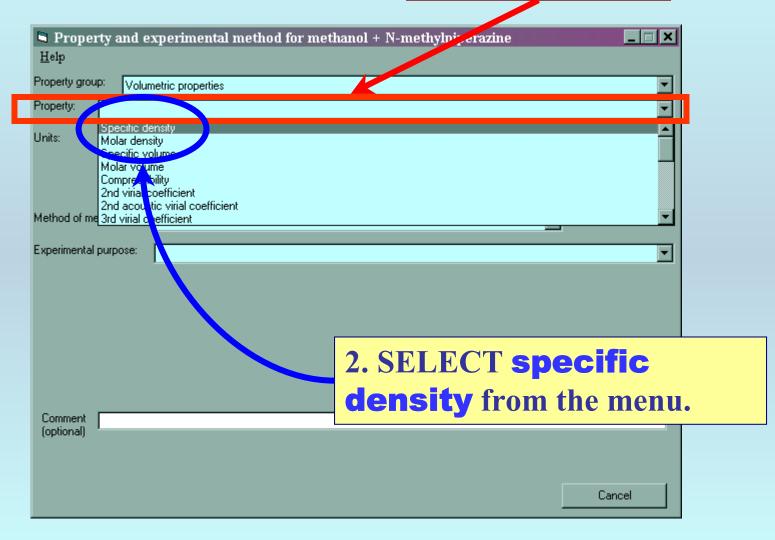
The data set considered here.

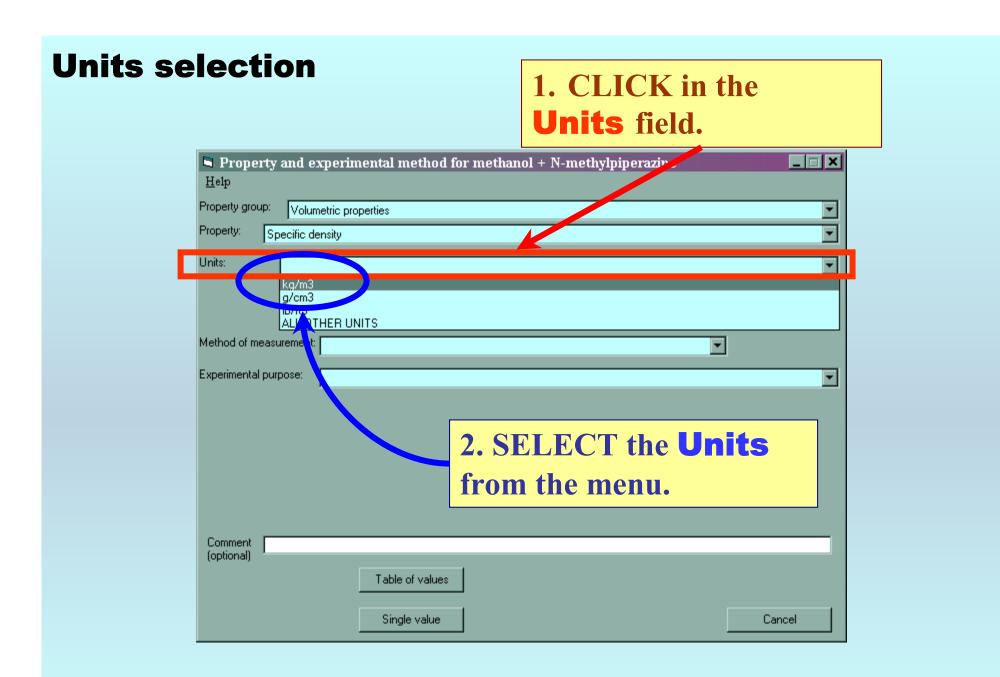


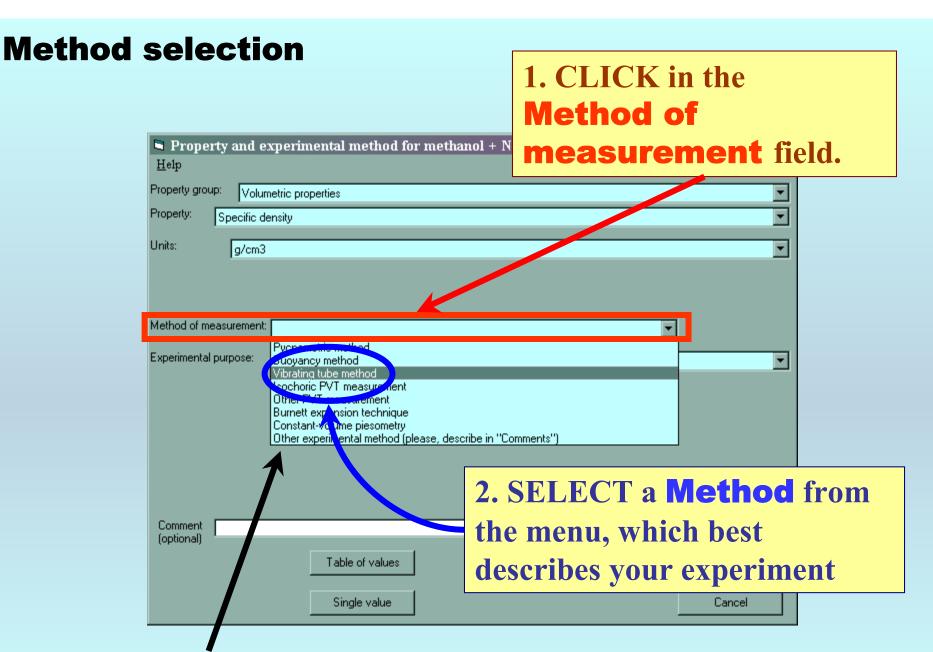
Property	Group selection
	<b>1. CLICK in the</b>
	property group field.
	Property and experimental method for methanol + N-taethylpiperazine Help
	Property group:
I	Vapor pressure; Boiling temperature; and Azeotropic T & P         Units:       Phase transition properties         Composition at press auilibrium         Activity; Fugacity;and Osmotic properties         Volumetric properties         Heat capacity and derived properties         Excess: partial; and upparent energetic properties
	Method of measurement:
	Experimental purpose:
	2. SELECT Volumetric
	properties from the menu.
	Comment (optional)
	Cancel

#### **Property selection**

# 1. CLICK in the **Property** field.

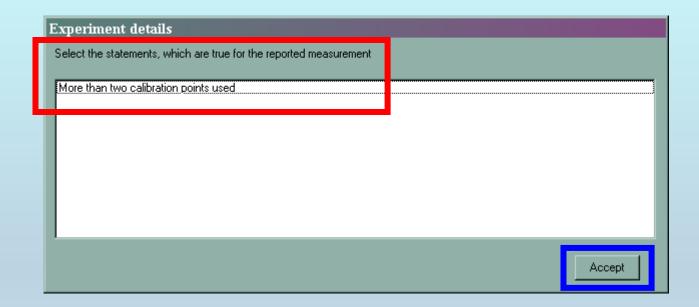






**Note:** *Other* is an option. A one sentence description or a reference is often adequate.

#### **Method detail selection**



# **Note:** For a few methods, additional details are requested. **SELECT** those statements that apply, and **CLICK** *Accept*.

#### **Experimental purpose selection**

Property and experimental method for me <u>Help</u> Property: Specific density	1. CLICK in the <b>Experimental purpose</b> field.
Units: g/cm3	
You are entering the data:	
<ul> <li>In original units (as in the source)</li> <li>In system units (</li> </ul>	converted)
Method of measurement: Vibrating tube method	
Experimental purpose: Principal objective of the work	
Principal objective of the work Secondary purpose (by-product of or Determined for identification or a syn	her objective) thesized compound
Comment (optional)	
	<b>2. SELECT the purpose</b> from the menu.

### Form is complete...

Property and experimental method for	r methanol + N-methylpiperazine	_ 🗆 🗙
Help		
Property group: Volumetric properties		-
Property: Specific density		•
Units: g/cm3		<b>_</b>
Method of measurement: Vibrating tube method	D	etails
Experimental purpose: Principal objective of the work	<	
	1. CLICK <i>Table of values</i>	
C		
Comment (optional) Table of values		
Single value	Ca	ancel

#### **Specification of phases and constraints**

Specific density as function of 1 variable(s)			×
Mixture: methanol + N-methylpiperazine			
Phases in equilibrium: 1 Constraints: T Independent variables: Phase of the Property Value(s) 2		Property set # 1 Sample # 1 Sample # 1 Precision of the Property Value(s)	%
	-		
1. SELECT # of Phases		2. SELECT # of <b>Constraints</b>	
from the pulldown list:		from the pulldown list:	
(one here - liquid)		(two here – T and p)	
- Definition of Measurement Hesults (Absolute vs Helative)	- -		
Data presentation			
Comments (Optional):			
Property and method		Numerical Data Cancel	

Specific density (kg/m3) as function of 1 variable(s)	
Mixture: methanol + N-methylpiperazine Phases in equilibrium: 1 Constraints: Independent variables: 1 Phase of the Property Value(s)	Property set # 1 Sample # 1 Sampl
<b>NOTE:</b> # of variables is calculated automatically based upon the Gibbs phase rule.	<b>NOTE:</b> If there is more than one sample for the components, the sample # can be specified here. <i>(This is rare.)</i>
Data presentation Experimental values	
Comments (Optional): Property and method	Numerical Data Cancel

#### Phase of the property value selection

Specific density (g/cm3) as function of 1 variable(s)	
Mixture: methanol + N-methylpiperazine	
Phase of the Property Val. (a) Classs Class of pure methanol Glass of pure N-methylpiperazine Liquid Circuit Class of pure N-methylpiperazine	erty set # 1 Sample # 1 Sample # 1 Precision of the Property Value(s)  Precision of the Property Value(s)  g/cm3 %
Liquid of purple and an analysis and a second secon	<b>2. SELECT the Phase</b>
1. CLICK in the Phase of the Property Values field	associated with the property values from the menu; ( <i>liquid</i> here).
Comments (Optional): Property and method	Numerical Data Cancel

Specific density (kg/m3) as function of 1 va	ariable(s)				
Mixture: methanol + N-methylpiperazine Phases in equilibrium: 1 Constraints: 2 -	Independent variables:	Property set # 1	Sample # 1 🔻 Sampl	e # [4 ]	▼
				n of the Property Value(s)	
Phase of the Property Value(s) Liquid				⊙ kg/m3	0 %
- Constraint 1 (Fixed value of)	▼ of	<b></b>	Units:	Uncertainty:	-
- Constraint 2 (Fixed value of)			l		
	▼ of		Units:	Uncertainty:	
- Independent variable 1			Units:	Uncertainty:	
1	▼ of			Uncertainty:	
Definition of Measurement Results (Absolute vs Relative)					
		IOTE: Fiel	ds for spec	ification of	
Data presentation		onstraints, v	_		
Experimental values				<i>,</i>	
	U	ncertainties	s, appear at	itomatically	
Comments (Optional):	h	ased on the	Gibbs Phas	se Rule	
	Property and method		Numerical Data	Cancel	

#### Variable and constraint identification

Specific density (g/cm3) as function of 1 variab	le(s)				
Mixture: methanol + N-methylpiperazine					-
Phases in equilibrium: 1 🔽 Constraints: 2 💌 I	ndependent variables: 1	Property set # 1	Sample # 1 Sample # 1	•	
			Precision of th	e Property Value(s)	<b>C N</b>
Phase of the Property Value(s) Liquid	_			⊙ g/cm3	0 %
Constraint 1 (Fixed value of)					
Temperature	i I-quia	Value:	Units: K	Uncertainty:	
Constraint 2 (Fixed value of)					
Pressure	n Prânia	Vole:	Units:	Uncertainty:	
Independent variable 1					
	<sup>of</sup> Liquid		Units:	Uncertainty:	
Temperature Arrows					
Partial pressure of methanol Partial pressure of N-methylpiperazine					
Partial pressure of component 3 Mole fraction of methanol					
Mole fraction of N-methylpiperazine Weight fraction of methanol		Identify Co	onstraints	5	
		• • • • • • • • • • • • • • • • • • •			
Data presentation		and varia	<b>bles</b> from	tne	
Experimental values		manus near	ridad		
	l l l l l l l l l l l l l l l l l l l	menus prov	lueu.		
Comments (Optional):					
Pro	perty and method		Numerical Data Ca	incel	

#### **Entry of values for constraints**

Specific density (g/cm3) as function of 1 variable(	(s)		_ 🗆 🗙
Mixture: methanol + N-methylpiperazine			•
Phases in equilibrium: 1 🔽 Constraints: 2 💌 Inde	ependent variables: 1 Property set # 1 Sam	ple # 1 💌 Sample # 1 💌	
		Precision of the Property Value(s)	-
Phase of the Property Value(s) Liquid		g/cm3	0 %
Constraint 1 (Fixed value of)			
Temperature of	Liquid Value: 298.15	Units: K Uncertainty:	
Constraint 2 (Fixed value of)			
Pressure of	Liquid Value: 1	Units: U certainty:	
-Independent variable 1		kPa MegaPa	
Mole fraction of methanol 🗾 of		Units: Pa Un ertainty:	
		kbar	
		bar kg/cm2	
□ Definition of Measurement Results (Absolute vs Relative)	·	Ib/in2 (psia)	
	<u> </u>		
Data presentation			
Experimental values			
	TYPE Values f	for the	
Comments (Optional):	<b>Constraints and S</b>		
	constraints and s		
Property	<sup>ya</sup> <b>lipite</b> from the		
	<b>Units</b> from the	menus.	

#### **Capture of precisions, if known**

🖣 Specific density (g/cm3) as function of 1 va	uriable(s)				
Mixture: methanol + N-methylpiperazine					-
Phases in equilibrium: 1 🔽 Constraints: 2 💌	Independent variables: 1	Property set # 1	Sample # 1 💽 Sample	#1 ▼	
Phase of the Property Value(s) Liquid			- Precision	of the Property Value(s) © g/cm3	0 %
Constraint 1 (Fixed value of)	of lue → u	Value: 200.15			
Temperature	of Liquid	Value: 298.15	Units: K	✓ Uncert tu [0.01]	
Constraint 2 (Fixed value of)		Value: It			
Pressure	of Liquid	Value: 1	Units: bar		□ %
Independent variable 1					
Mole fraction of methanol	of Liquid	•			
Definition of Measurement Results (Absolute vs Relative) —					
			s for the		
Data presentation Experimental values	<b>precisi</b>	ons of th	ne proper	ties,	
	variab	les, and	constrair	nts, if	
Comments (Optional):	<b>known</b>	•			
	Property and meanod		Hamonoar Bata	Cancer	

**NOTE:** Only the precision of temperature was provided by the authors in this example.

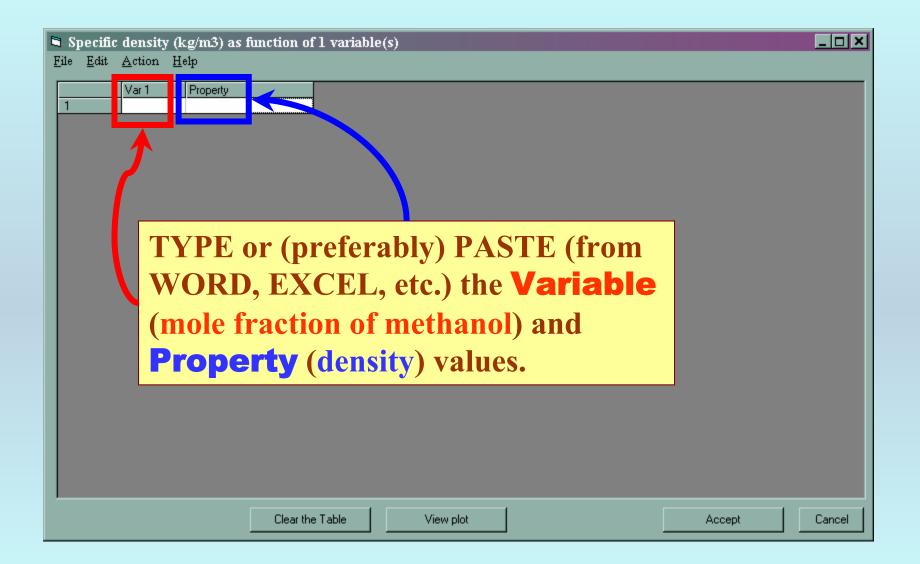
#### **Define results: Absolute vs Relative**

ixture: methanol + N-methylpiperazine   Phases in equilibrium:   1 Constraints:   Phase of the Property Value(s)   Liquid Image: Constraint 1 (Fixed value of)   Temperature   0 Liquid   Value:   298.15 Units:   K Uncertainty:   0.01 %   Independent variable 1   Nample # 1   SELECT Direct   Nite
Phase of the Property Value(s) Liquid  Phase of the Property Value(s) Liquid  Constraint 1 (Fixed value of)  Temperature  of Liquid  value: 298.15  Units: K  Uncertainty: 0.01  %  Constraint 2 (Fixed value of)  Pressure  of Liquid  SELECT Direct
Phase of the Property Value(s) Liquid
Constraint 1 (Fixed value of) Temperature Constraint 2 (Fixed value of) Pressure Pre
Temperature       of Liquid       Value: 298.15       Units: K       Uncertainty: 0.01       %         Constraint 2 (Fixed value of)       Pressure       of Liquid       SELECT Direct       ertainty: 100       %         Independent variable 1       SELECT Direct       %
Constraint 2 (Fixed value of) Pressure Independent variable 1 Pressure Pres
Pressure   Pressure  Pressure  SELECT Direct  Pressure  Pressure
Independent variable 1 SELECT Direct
Mole fraction of methanol 🔹 of Liquid 💌
<i>values</i> from the
Definition of Measurement Results (Absolute vs Relative) menu.
Direct value Rel. to ref. phase with same composition at FIXED T and P
Rel. to ref. phase with SAME composition, T and P
Rel. to mixture in EQUIL, with primary phase at same T and P Rel. to pure COMPONENTS in same proportion at same T and P
Rel. to pure SOLVENT at T of same phase EQUILIBRIUM Rel. to pure SOLVENT at same T and P
Rel. to pure SOLUTE at same T and P
Comments (Optional):
Property of method Numerical Data Cancel

**NOTE:** Other options are typically for data reported as relative values (e.g., relative to the density of the pure solovent). These are not common.

### Form is complete...

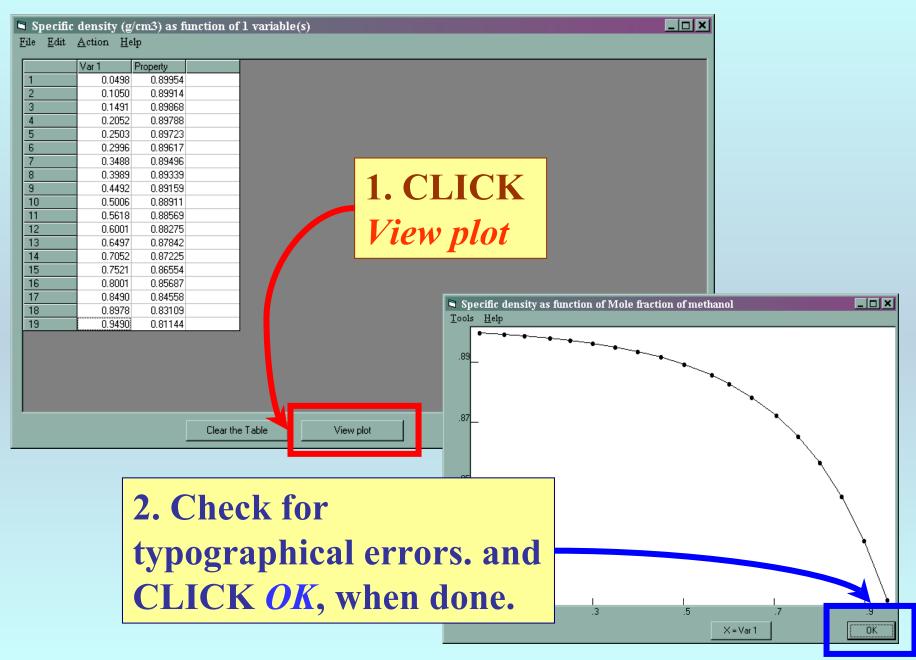
Specific density (g/cm3) as function of 1 variable(s)						
Mixture: methanol + N-methylpiperazine					•	
Phases in equilibrium: 1 🔽 Constraints: 2 💌	Independent variables: 1	Property set # 1	Sample # 1 💌 Sample # 1	•		
				Property Value(s)		
Phase of the Property Value(s) Liquid				⊙ g/cm3	0 %	
Constraint 1 (Fixed value of)						
Temperature	of Liquid	▼ Value: 298,15	Units: K	Uncertainty: 0.01		
Constraint 2 (Fixed value of)						
Pressure	of Liquid	▼ Value: 1	Units: bar	Uncertainty:		
Independent variable 1						
Mole fraction of methanol	of Liquid	<b>•</b>	Units: Dimensionless	Uncertainty:		
□ Definition of Measurement Results (Absolute vs Relative) ——						
Direct value			LICK			
Data presentation			imerical D	ata 🗖		
Experimental values	•					
Comments (Optional):						
	Descents and events and		Numerical Data			
	Property and method		Numerical Data Cano			



	Var 1	Property				VE			VE
1	0.0498	0.89954		<u></u> X1	$g cm^{-3}$	$\mathrm{cm}^3\cdot\mathrm{mol}^{-1}$	$x_1$	g∙cm <sup>−3</sup>	$\text{cm}^3 \cdot \text{mol}^{-1}$
2	0.1050	0.89914		Meth	nanol $(1) +$	NMP (2)	<i>n</i> -Pro	panol(1) +	· NMP (2)
3	0.1491	0.89868		0.0498	0.899.54	-0.225	0.0483	0.89802	-0.187
4	0.2052	0.89788		0.1050	0.899.14	-0.463	0.1012	$0.895\ 74$	-0.361
5	0.2503	0.89723		0.1491	0.898~68	-0.641	0.1395	0.89407	-0.492
6	0.2996	0.89617		0.2052	$0.897\ 88$	-0.848	0.1465	0.89378	-0.519
7	0.3488	0.89496		0.2503	0.897 23	-1.020	0.1950	0.891.38	-0.661
8	0.3989	0.89339		0.2996	0.896 17	-1.178	0.2439	0.88898	-0.815
9	0.4492	0.89159		0.3488	0.894 96	-1.330	0.2936	0.88606	-0.930
10	0.5006	0.88911		0.3989	$0.893 \ 39 \\ 0.891 \ 59$	-1.465	$0.3473 \\ 0.3914$	0.882 79 0.879 95	$-1.056 \\ -1.153$
11	0.5618	0.88569		0.4492	0.891 59	$-1.593 \\ -1.686$	0.3914 0.4476	0.879.95	-1.153 -1.255
12	0.6001	0.88275	 <u> </u>	0.5618	0.885 69	-1.686 -1.787	0.4476 0.4913	0.872 65	-1.255 -1.323
13	0.6497	0.87842		0.6001	0.882 75	-1.807	0.4313 0.5452	0.86803	-1.370
14	0.7052	0.87225		0.6497	0.878 42	-1.822	0.5934	0.863 55	-1.395
15 16	0.7521	0.86554		0.7052	0.872 25	-1.789	0.6424	0.85859	-1.399
16	0.8001	0.85687 0.84558		0.7521	0.865 54	-1.707	0.6922	0.85304	-1.372
17	0.8490	0.84558		0.8001	0.856 87	-1.563	0.7420	0.84678	-1.299
19	0.0370	0.83109		0.8490	0.845 58	-1.340	0.7941	0.83947	-1.177
13	0.5450	0.01144		0.8978	0.831 09	-1.023	0.8425	0.831~79	-1.006
			4	0.9490	0.81144	-0.571	0.8954	0.822 30	-0.749
							0.9474	0.81176	-0.419

*Type* or (preferably) *Paste* from WORD, EXCEL, etc.

#### **Graphical check for typographical errors**

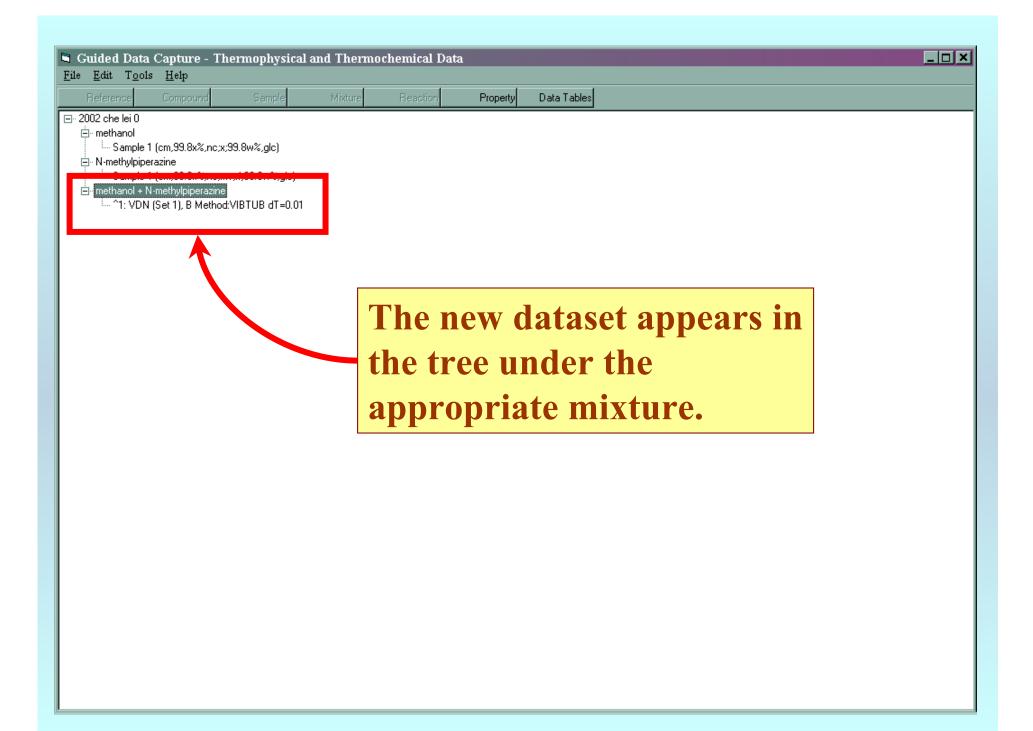


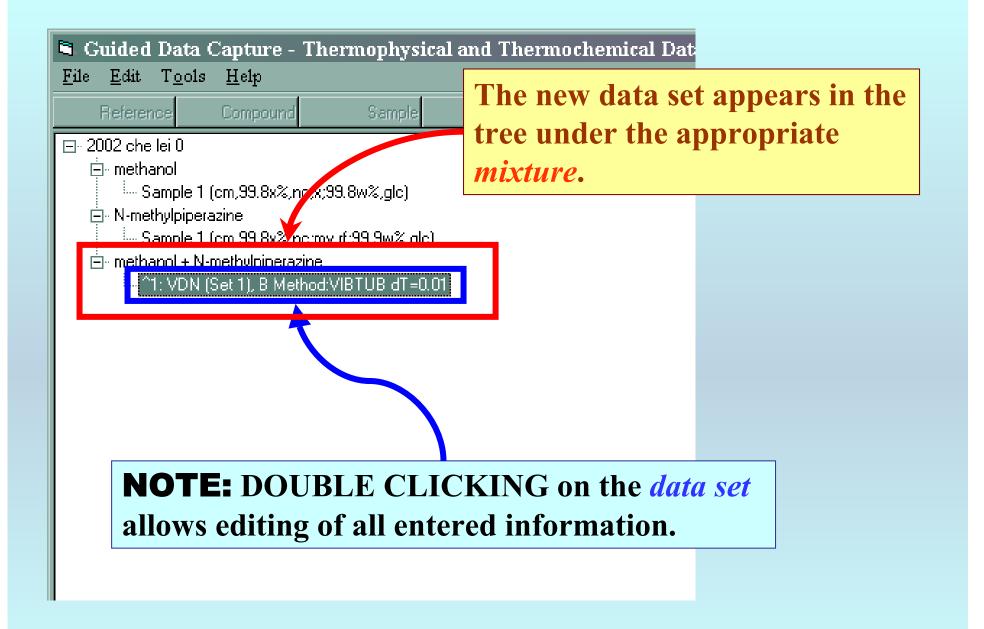
# **NOTE:** The plots have several useful features. See the *HELP* screen on the plot.

🤣 Guided Data Capture								
<u>F</u> ile <u>E</u> dit Book <u>m</u> ark <u>O</u> ptions <u>H</u> elp								
Contents	Index	<u>B</u> ack	<u>P</u> rint	<u>&lt;</u> <	≥>			
GRAPH COMMANDS								
Use available buttons to select mode								
Esc, Enter keys, or OK button to close								
Click on a point to view its coordinates								
Double click on a point to go to the corresponding data								
If you wish to view only a part of the data set, select the range of cells in the parent								
form before clicking "View Plot"								
Click, drag and release the mouse button to magnify a part of the plot								

### **Final acceptance**

Specific <u>File E</u> dit	c density (g/cm3) as i <u>A</u> ction <u>H</u> elp	nction of 1 variable(s)		<u>_     ×</u>
	Var 1 Property			
1	0.0498 0.89954			
2	0.1050 0.89914			
3	0.1491 0.89868			
4	0.2052 0.89788			
5	0.2503 0.89723			
6	0.2996 0.89617			
7	0.3488 0.89496			
8	0.3989 0.89339			
9	0.4492 0.89159			
10	0.5006 0.88911			
11	0.5618 0.88569			
12	0.6001 0.88275			
13	0.6497 0.87842			
14	0.7052 0.87225		CK Accept	
15	0.7521 0.86554		<b>NACCEPI</b>	
16	0.8001 0.85687		<b>4</b>	
17	0.8490 0.84558			
18	0.8978 0.83109			
19	0.9490 0.81144			
		Clear the Table View plot	Accept	Cancel







**Continue with other compounds, samples, properties, reactions, etc...** 

or save your file and exit the program.