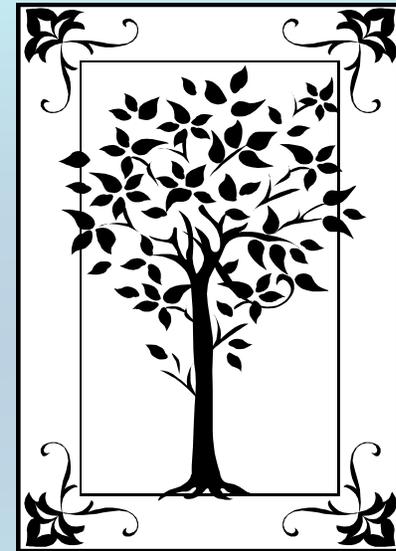


**METADATA AND NUMERICAL DATA CAPTURE:
VLE (Txy) data
(3 components)**

***Guided Data
Capture (GDC)***



This tutorial describes
METADATA AND NUMERICAL DATA CAPTURE:
for **VLE (Txy) data**
Composition at phase equilibrium
with the Guided Data Capture (GDC) software.

NOTE:

The tutorials proceed sequentially to ease the descriptions. **It is not necessary to enter *all* compounds before entering *all* samples, etc.**

Compounds, samples, properties, etc., can be added or modified at any time.

However, the hierarchy must be maintained (i.e., a property cannot be entered, if there is no associated sample or compound.)

The experimental data used in this example is from:

JE0301460

VLE (T, x_1, x_2, y_1, y_2) for a 3-component mixture (*ethanol + cyclohexane + water*)

Table 2 VLE Data for ethanol(1)/cyclohexane(2)/water(3) System

$t/^\circ\text{C}$	mole fraction in liquid phase		mole fraction in vapor phase	
	x_1	x_2	y_1	y_2
35	0.5096	0.4257	0.2948	0.6352
	0.5776	0.3814	0.3269	0.6251
	0.5972	0.3589	0.3201	0.6325
	0.6675	0.2752	0.3381	0.6116
	0.7155	0.2137	0.3369	0.6095
	0.7066	0.1073	0.3213	0.5809
	0.8100	0.0973	0.4101	0.5302
	0.8457	0.0678	0.4795	0.4640
	0.4790	0.0046	0.4651	0.2965
50	0.4902	0.4886	0.3887	0.5754
	0.5542	0.4095	0.3881	0.5668
	0.5825	0.3746	0.3861	0.5588
	0.6411	0.3065	0.3957	0.5503
	0.6885	0.2439	0.4043	0.5344
	0.7703	0.1121	0.4274	0.4915
	0.8324	0.0766	0.5229	0.4075
	0.6749	0.1437	0.3603	0.5513
	0.6753	0.0682	0.4049	0.4525
	0.5982	0.0263	0.4332	0.3647
0.4644	0.0103	0.3796	0.4190	
65	0.8276	0.0786	0.5584	0.3672
	0.6822	0.0603	0.4141	0.4379
	0.8650	0.0405	0.6221	0.3027
	0.8060	0.1113	0.5175	0.4174
	0.8098	0.1288	0.5057	0.4418
	0.7160	0.2370	0.4572	0.4957
	0.6124	0.3523	0.4271	0.5244
	0.5653	0.4041	0.4204	0.5327

These data are considered here.

Results are reported for 3 temperatures.

Experimental Method Info:

Compositions are determined by gas chromatography

Guided Data Capture - Thermophysical and Thermochemical Data

File Edit Tools Help

Reference Compound Sample Mixture Reaction **Property** Data Tables

- 2003 cui qia 0
 - water
 - Sample 1 (cm,fd;99.9m%,est)
 - ethanol
 - Sample 1 (cm,99.5x%,nc;dc,fd;)
 - cyclohexane
 - Sample 1 (cm,99.5v%,nc;dc,fd;)
 - ethanol + cyclohexane + water**

2. CLICK *Property*

1. SELECT the *mixture* for which the data are to be captured.

NOTE: The **bibliographic information, compound identities, sample descriptions, and mixture** were entered previously. (There are separate tutorials, which describe capture of this information, if needed.)

Property and experimental method for ethanol + cyclohexane + water

Help

Property group: Composition at phase equilibrium

Property: Mole fraction of cyclohexane

Units: Dimensionless

Method of measurement:

Experimental purpose:

Comment
(optional)

OK

Cancel

1. SELECT the **Property Group**:
Composition at phase equilibrium
from the menu.

2. SELECT the **Property**: *Mole fraction of cyclohexane*, for the example.

3. SELECT the **Units**:
Dimensionless in this case.

1. SELECT **Method of Measurement** from the list provided. **NOTE:** *Other* can be a valid selection and should include a brief description in the **Comment** field.

Units: Dimensionless

Method of measurement: Chromatography

Experimental purpose: Principal objective of the work

2. SELECT the **Experimental Purpose** from the list provided.

Comment (optional)

3. CLICK *OK*

OK

Cancel

SELECTION of # of Phases in Equilibrium and # of Constraints

Mole fraction of cyclohexane () (Dimensionless) as function of 3 variable(s)

Mixture: ethanol + cyclohexane + water

Phases in equilibrium: 2

Constraints: 0

Independent variables: 3

Phase of the Property Value(s)

SELECT the # of **Phases in equilibrium**. There are **2** in the example; *liquid* and *gas*.

SELECT the # of **Constraints** (such as *temperature, pressure, or composition*). There are none in the example.

Specific density (g/cm³) as function of 3 variable(s)

Mixture: 2,5,8,11,14-pentaoxapentadecane + 1,1,1,2-tetrafluoroethane

Phases in equilibrium: 1 Constraints: 0 Independent variables: 3 Property set #: 1

Sample #: 1 Sample #: 1

Phase of the Property Value(s):

Position of the Property Value(s): g/cm³ %

Definition of Measurement Results (Absolute vs Relative):

Data presentation: Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

Multiple *samples* for a given component can be accommodated, but this is rarely needed.

Mole fraction of cyclohexane (Gas) (Dimensionless) as function of 3 variable(s)

Mixture: ethanol + cyclohexane + water

Phases in equilibrium: 2 Constraints: 0 Independent variables: 3 Property set # 1 Sample # 1 Sample # 1 Sample # 1

Phase of the Property Value(s) Gas Precision of the Property Value(s) Dimensionless %

Phase 2:

Independent variable 1:

Independent variable 2:

Independent variable 3:

Definition of Measurement Result (Absolute vs Relative)

Data presentation: Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

1) SELECT *Gas* from the list provided for the **Phase of the Property Value**.

NOTE: In this example, y_2 is captured as a function of T , x_1 , and x_2 . A second data set (y_1 as a function of T , x_1 , and x_2) should be captured separately.

NOTE: Constraint and Independent Variable field(s) appear automatically based on the entered information and the *Gibbs Phase Rule*.

1. SELECT **Phase 2, Liquid**, and the **Independent Variable(s)** from the menus.

Mixture: ethanol + cyclohexane + water

Phases in equilibrium: 2 Constraints: 0 Independent variables: 3 Property set # 1 Sample # 1 Sample # 1 Sample # 1

Phase of the Property Value(s) Gas

Precision of the Property Value(s)
 Dimensionless %

Phase 2
Liquid

Independent variable 1
Temperature of Liquid Units: C Uncertainty: %

Independent variable 2
Mole fraction of ethanol of Liquid Units: Dimensionless Uncertainty: %

Independent variable 3
Mole fraction of cyclohexane of Liquid Units: Dimensionless Uncertainty: %

Definition of Measurement Results (Absolute vs Relative)

Da
Ex

2. SELECT **Units** for the **Variable(s)** and **Values** for constraints, if required. Include approximate **Uncertainties** and **Precisions**, if known.

Property and method Numerical data Cancel

1. SELECT *Direct Value* (as compared with *Relative Value*) from the list defining the **Measurement Results**

2. SELECT the appropriate **Data presentation** method. *Experimental values* here.

3. CLICK *Numerical Data*

Mole fraction of cyclohexane (Gas) (Dimensionless) as function of 3 variable(s)

Mixture: ethanol + cyclohexane + water

Phases in equilibrium: 2 Constraints: 0 Independent variable 1

Phase of the Property Value(s) Gas

Phase 2 Liquid

Independent variable 1 Temperature of Liquid

Independent variable 2 Mole fraction of ethanol of Liquid Units: Dimensionless Uncertainty: %

Independent variable 3 Mole fraction of cyclohexane of Liquid

Definition of Measurement Results (Absolute vs Relative)
Direct value

Data presentation
Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

Mole fraction of cyclohexane (Dimensionless) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1				
2				
3				
4				
5				
6				
7				
8				
9				
10				

Clear the Table View

TYPE, or much preferably, PASTE the variable and property values into the table. See next page...

Table 2 VLE Data for Ethanol(1)-Cyclohexane(2)-Water(3) System

t/C	mole fraction in liquid phase		mole fraction in vapor phase	
	x ₁	x ₂	y ₁	y ₂
35	0.5096	0.4257	0.2948	0.6352
	0.5776	0.3814	0.3269	0.6251
	0.5972	0.3589	0.3201	0.6325
	0.6675	0.2752	0.3381	0.6116
	0.7155	0.2137	0.3369	0.6095
	0.7066	0.1073	0.3213	0.5809
	0.8100	0.0973	0.4101	0.5302
	0.8457	0.0678	0.4795	0.4640
	0.4790	0.0046	0.4651	0.2965
50	0.4902	0.4886	0.3887	0.5754
	0.5542	0.4095	0.3881	0.5668
	0.5825	0.3746	0.3861	0.5588
	0.6411	0.3065	0.3957	0.5503
	0.6885	0.2439	0.4043	0.5344
	0.7703	0.1121	0.4274	0.4915
	0.8324	0.0766	0.5229	0.4075
	0.6749	0.1437	0.3603	0.5513
	0.6753	0.0682	0.4049	0.4525
65	0.5982	0.0263	0.4332	0.3647
	0.4644	0.0103	0.3796	0.4190
	0.8276	0.0786	0.5584	0.3672
	0.6822	0.0603	0.4141	0.4379
	0.8650	0.0405	0.6221	0.3027
	0.8060	0.1113	0.5175	0.4174
	0.8098	0.1288	0.5057	0.4418
	0.7160	0.2370	0.4572	0.4957
	0.6124	0.3523	0.4271	0.5244
0.5653	0.4041	0.4204	0.5327	

Mole fraction of cyclohexane (Dimensionless) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	35.0	0.5096	0.4257	0.6352
2	35.0	0.5776	0.3814	0.6251
3	35.0	0.5972	0.3589	0.6325
4	35.0	0.6675	0.2752	0.6116
5	35.0	0.7155	0.2137	0.6095
6	35.0	0.7066	0.1073	0.5809
7	35.0	0.8100	0.0973	0.5302
8	35.0	0.8457	0.0678	0.4640
9	35.0	0.4790	0.0046	0.2965
10	50.0	0.4902	0.4886	0.5754
11	50.0	0.5542	0.4095	0.5668
12	50.0	0.5825	0.3746	0.5588
13	50.0	0.6411	0.3065	0.5503
14	50.0	0.6885	0.2439	0.5344
15	50.0	0.7703	0.1121	0.4915
16	50.0	0.8324	0.0766	0.4075
17	50.0	0.6749	0.1437	0.5513
18	50.0	0.6753	0.0682	0.4525
19	50.0	0.5982	0.0263	0.3647
20	50.0	0.4644	0.0103	0.4190
21	65.0	0.8276	0.0786	0.3672
22	65.0	0.6822	0.0603	0.4379
23	65.0	0.8650	0.0405	0.3027
24	65.0	0.8060	0.1113	0.4174
25	65.0	0.8098	0.1288	0.4418

Clear the Table View plot

Paste the table of values into the form

Table 2 VLE Data for Ethanol(1)-Cyclohexane(2)-Water(3) System

T/C	mole fraction in liquid phase		mole fraction in vapor phase	
	x_1	x_2	y_1	y_2
35	0.5096	0.4257	0.2948	0.6352
	0.5776	0.3814	0.3269	0.6251
	0.5972	0.3589	0.3201	0.6325
	0.6675	0.2752	0.3381	0.6116
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	0.4644	0.0103	0.3796	0.4190
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	0.6822	0.0603	0.4141	0.4379
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	0.8060	0.1113	0.5175	0.4174
	0.8098	0.1288	0.5057	0.4418
	0.7160	0.2370	0.4572	0.4957
	0.6124	0.3523	0.4271	0.5244
0.5653	0.4041	0.4204	0.5327	

NOTE: Simple CUT/PASTE procedures can be used within the table to convert the original table into the required number of columns. (This can also be done externally in spreadsheet software, e.g., EXCEL.)

Mole fraction of cyclohexane (Dimensionless) as function of 3 variable(s)

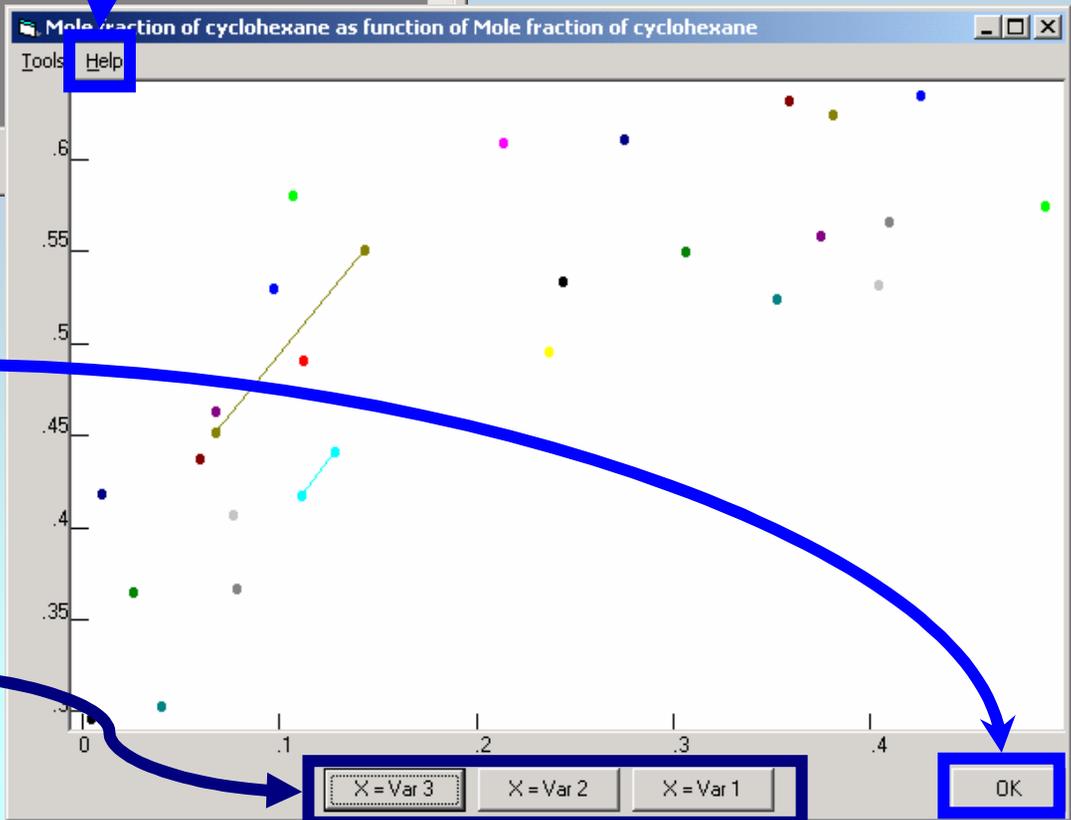
File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	35.0	0.5096	0.4257	0.6352
2	35.0	0.5776	0.3814	0.6251
3	35.0	0.5972	0.3589	0.6325
4	35.0	0.6675	0.2752	0.6116
5	35.0	0.7155	0.2137	0.6095
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22	65.0	0.6822	0.0603	0.4379
23	65.0	0.8650	0.0405	0.3027
24	65.0	0.8060	0.1113	0.4174
25	65.0	0.8098	0.1288	0.4418

Clear the Table View plot

1. CLICK *View plot* to see a graphical representation of the data.

NOTE: See **HELP** for addition graph commands.



2. Check for typographical errors, and CLICK *OK*, when done.

NOTE: These buttons provide different views of the data.

Mole fraction of cyclohexane (Dimensionless) as function of 3 variable(s)

File Edit Action Help

	Var 1	Var 2	Var 3	Property
1	35.0	0.5096	0.4257	0.6352
2	35.0	0.5776	0.3814	0.6251
3	35.0	0.5972	0.3589	0.6325
4	35.0	0.6675	0.2752	0.6116
5	35.0	0.7155	0.2137	0.6095
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14	50.0	0.6885	0.2439	0.5344
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24	65.0	0.8060	0.1113	0.4174
25	65.0	0.8098	0.1288	0.4418

CLICK *Accept*

Clear the Table View plot **Accept** Cancel

Guided Data Capture - Thermophysical and Thermochemical Data

File Edit Tools Help

Reference

Compound

Sample

- [-] 2003 cui qia 0
 - [-] water
 - ... Sample 1 (cm;fd;99.9m%,est)
 - [-] ethanol
 - ... Sample 1 (cm,99.5x%,nc;dc,fd;)
 - [-] cyclohexane
 - ... Sample 1 (cm,99.5x%,nc;dc,fd;)
 - [-] ethanol + cyclohexane + water

^3: vle, X2 (G, Set 1), B Method:CHROM

NOTE: The new data set now appears in the tree under the appropriate *mixture*.

NOTE: DOUBLE CLICKING on the *data set* allows editing of all entered information.

END

Continue with other *compounds*,
samples, *properties*, *reactions*, etc...

or save your file and exit the program,
if all properties have been captured.