

# Early LNG Program and LN<sub>2</sub> Cryogenic Flow Measurement Facility at NIST

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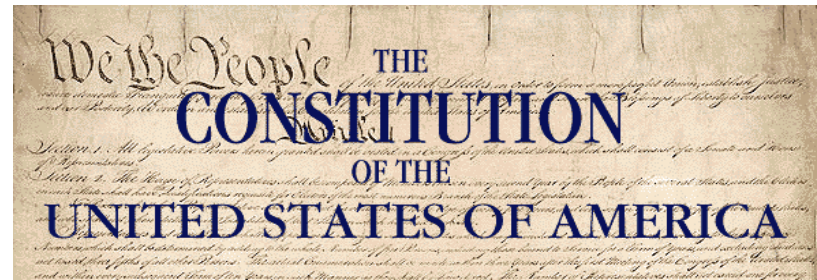
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LNG Metrology Workshop  
9 November 2010  
Stockholm, Sweden

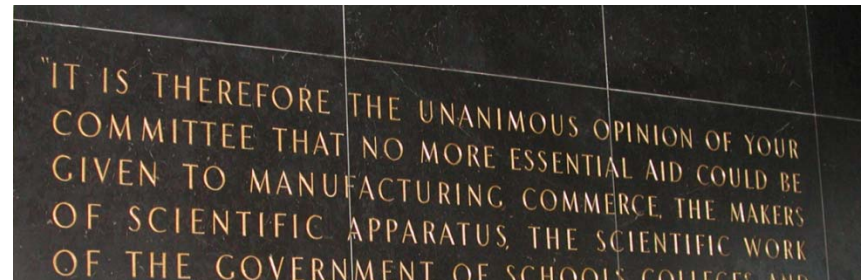
# National Institute of Standards and Technology (NIST)

*NIST is the National Metrology Institute (NMI) for the U.S., and signatory to the CIPM MRA*

- Non-regulatory agency within U.S. Department of Commerce
- Founded in 1901 as National Bureau of Standards



**Article I, Section 8: The Congress shall have the power to ...*coin money, regulate the value thereof, and of foreign coin, and fix the standard of weights and measures***



## **Mission ...**

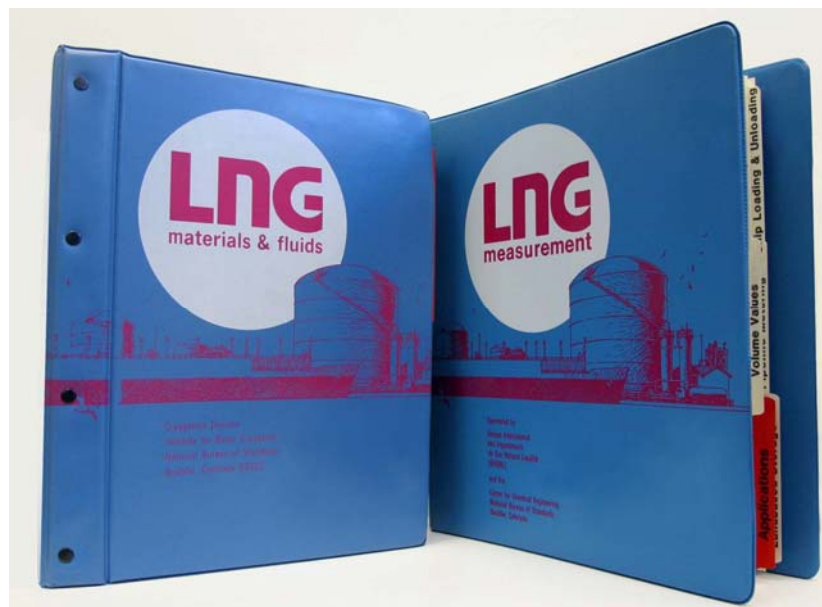
**to promote U.S. innovation and industrial competitiveness by advancing measurement science, standards, and technology**

**in ways that enhance economic security and improve our quality of life**

# LNG at NIST (NBS): 1970 to 1985

## Sponsors and Collaborators

- Groupe International des Importateurs de Gaz Naturel Liquéfié
- American Gas Association
- Gas Research Institute
- DOC Maritime Administration
- American Bureau of Shipping
- ...



- Western LNG Terminal Assoc.
- Tokyo Gas Co.
- Columbia LNG Corp.
- El Paso LNG Co.
- Ruhrgas LNG
- ...

# LNG Materials and Fluids

- Materials

- Structural Materials: Aluminum Alloys; Invar; Nickel Steels, ...
- Thermal Insulators: Polystyrene; Polyvinyl Chloride; Balsa, ...
- Concrete: Elastic (Young's Modulus); Thermal; Mechanical
- Nonmetallic Laminates: Cotton fabric/phenolic; glass mat/epoxy

- Fluids

- Pure Fluids: methane, ethane, ... (charts, etc.)
- Fluid Mixtures: LNG mixtures, binary mixtures

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See: Cryogenic Material Properties Database (NIST SRD #152)  
<http://www.cryogenics.nist.gov/MPropsMAY/materialproperties.htm>  
NIST Chemistry WebBook (NIST SRD #69)  
<http://webbook.nist.gov/chemistry/>  
NIST REFPROP (NIST SRD #23)  
<http://www.nist.gov/srd/nist23.cfm>

# LNG Measurement

*A User's Manual for Custody Transfer (1985)*

## Section 1

- Physical Properties
  - SI System
  - Pure Fluid Properties
  - Combustion Enthalpies





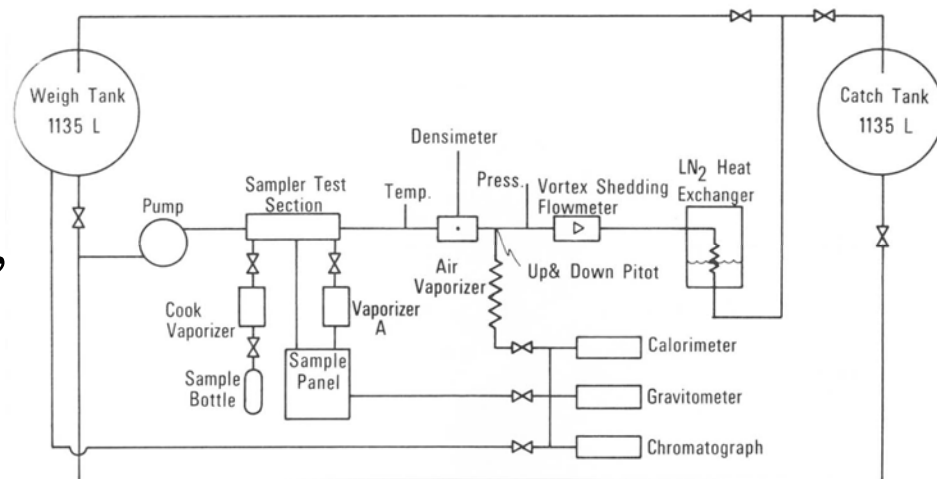
# LNG Measurement

- Measurement Elements
  1. Measurement Process Applied to LNG
  2. Sampling and Analysis
    - Sample probe (pitot, side tube, ...)
    - Sample conditioner (vaporizing)
    - Gas analyzer (GC, MS, integrator, packings, etc. )
    - Operating parameters/procedures



Laboratory tests  
LNG Flow Loop  
Shipboard Tests (at Canvey Island,  
England)

$U(3\sigma, \text{heating value}) = 0.3 \%$



# LNG Measurement

- Measurement Elements

- 3. Calorific Value: *calorimeters, calculations, comparisons*

- 4. Density Values:

- Cryogenic density reference system—*calibrations of LNG densimeter transfer standards*  $U(\text{LCH}_4) = 0.055\%$

- Portable Reference Densimeter—*tests of commercial LNG densimeters*

- Experimental LNG Density—*NBS densimeters; pure fluids; binary mixtures, multicomponents* (NBS Monograph 172, 1983)

- Mathematical Models for LNG Densities—*ECS, HS, Klosek & McKinley (r), cell*

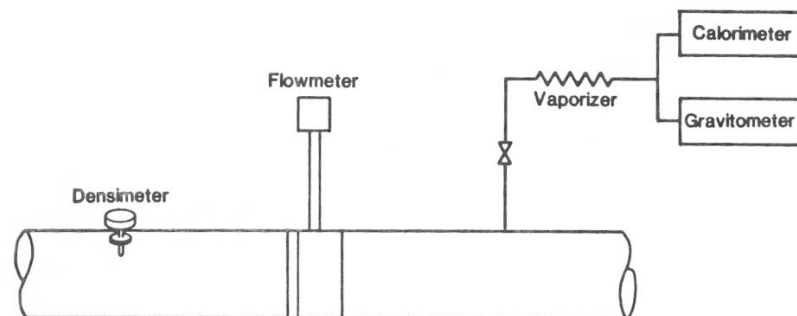
See: ASTM D4784 – 93 (2010) *Standard Specification for LNG Density Calculation Models*  
GERG EOS (2004)  
NIST REFPROP (NIST SRD #23) <http://www.nist.gov/srd/nist23.cfm>

# LNG Measurement

- Measurement Elements

- 5. LNG Volume

- Liquid Level Measurement: *capacitance gauges, cable gages, bubbler gauges*
- Volume of Membrane-Type LNG Ship Tanks  $U = 0.1 \%$
- Volume of Freestanding Prismatic LNG Ship Tanks  $U = 0.1 \%$
- Volume of Spherical LNG Ship Tanks
- Volume of Cylindrical LNG Shore Tanks  $U = 0.005 \%$
- Volume from Totalized Flow Rate Metering
  - LNG Measurement Station: *flowmeter, densimeter, calorimeter, gravitometer*  
5 cm to 81 cm (2 in to 32 in) flow meter scaleup





# LNG Measurement

- Applications

- Measurement Uncertainties: *volume, gas analysis (0.09 %), calculated LNG density (0.23 %), measured density (0.26 %), calculated calorific value (0.77 %), measured calorific value (0.77 %)*
- Ship Loading/Unloading (0.2 % to 0.4 % calorific value)
- Pipeline Metering (0.65 % to 0.95 %)
- Landbased Storage (0.34 % to 0.65 %)

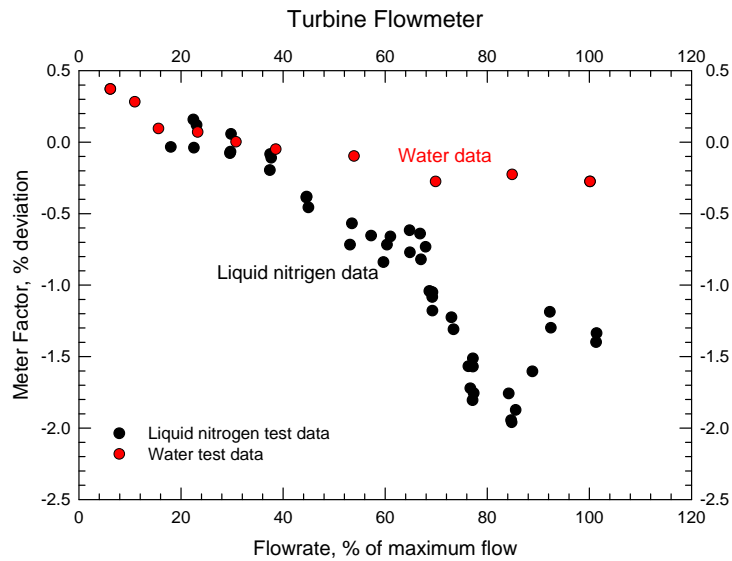
Estimates of Measurement Error  
LNG Measurement Process

LNG Measurement Element	Total Uncertainty (percent)	
	Measured	Calculated
Density	± 0.26	± 0.23
Calorific Value	± 0.77	± 0.35

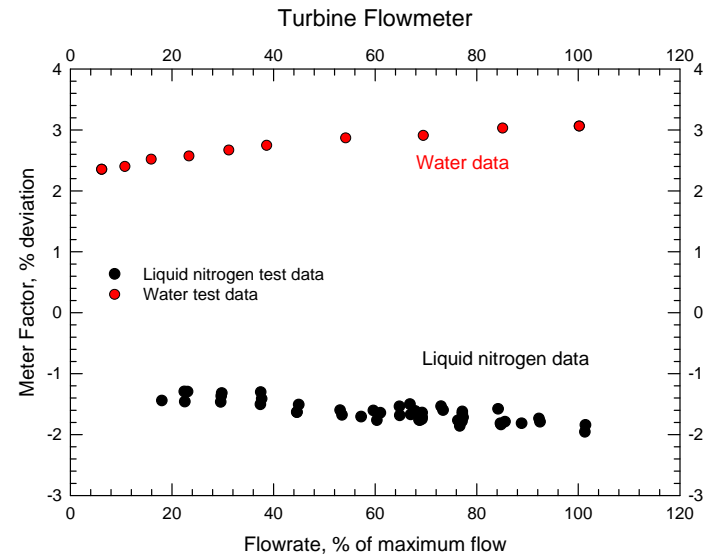
# NIST Cryogenic Flow Measurement Facility

Testing and Calibration Services

- Why LN<sub>2</sub> Calibrations?



- LN<sub>2</sub> vs Water Calibrations



# Capabilities

## Flow Rate

- Mass : 0.95 to 9.5 kg/s
- Volume : 1.26 to 12.6 L/s

## Absolute Pressure

- 0.4 to 0.76 MPa

## Temperature

- 80 to 90 K

# Metering Characteristics

- Meter Test Section Design
  - 25 to 150 mm diameter
  - 4 meter length
- Flowmeter Calibration Services
  - Turbine
  - Coriolis
  - Ultra Sonic
  - Vortex shedding
- Research Application
  - Prototype meter testing
  - Meter verification at LN<sub>2</sub> temperatures
- All measurements are traceable to national standards

# NIST Quality System and Conformance to ISO/IEC 17025

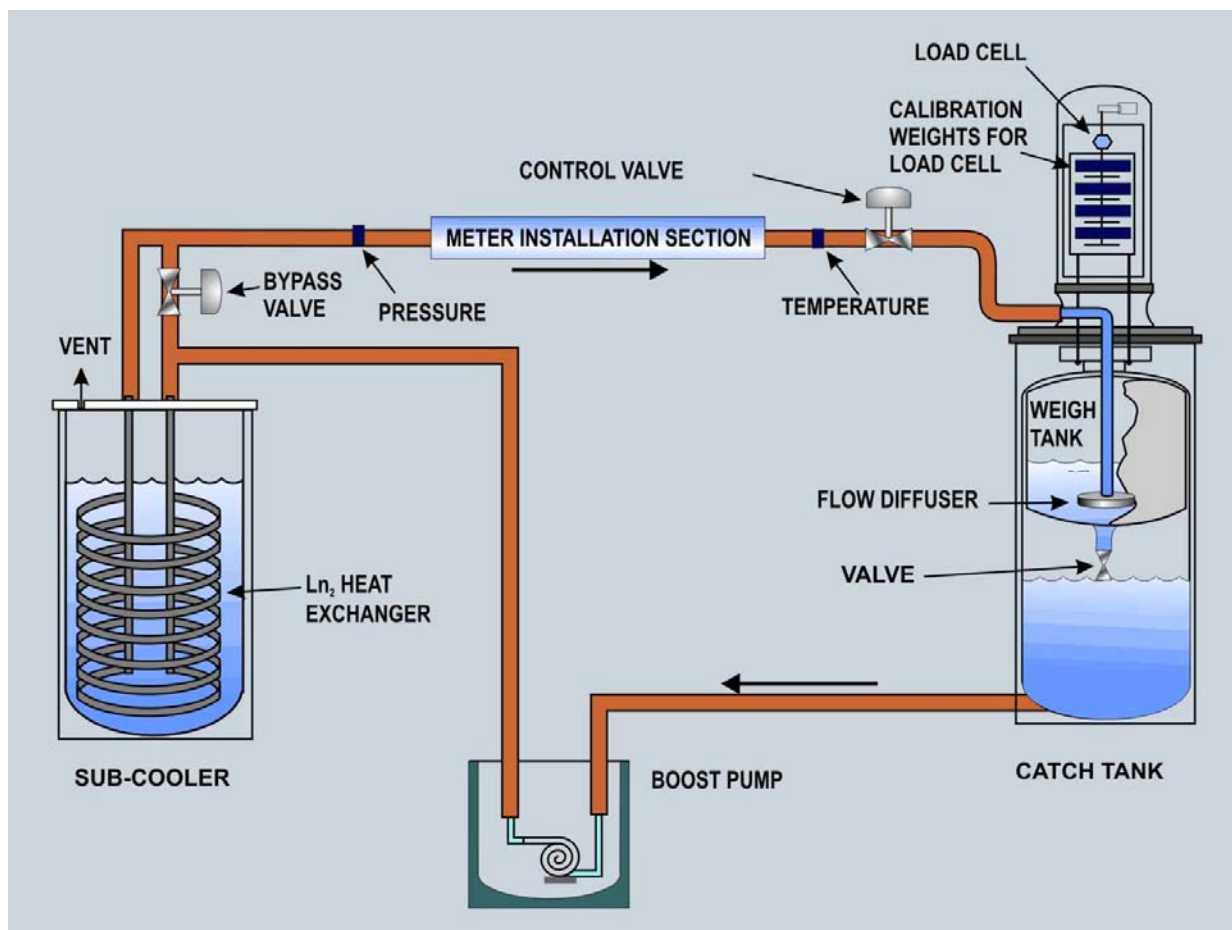
- NIST Quality System in place
- Website: <http://www.nist.gov/qualitysystem/>
- NIST Quality Assessment
- NIST Assessment Review Board
- NIST Measurement Services Advisory Group (MSAG)
- SIM Regional Metrology Organization
- QSTF: Quality Systems Task Force
- BIPM: Bureau International des Poids et Mesures
- CIPM: International Committee for Weights and Measures/ Comité International des Poids et Mesures
- MRA: Mutual Recognition Agreement
- CMC: Calibration and Measurement Capabilities
- Inclusion in Appendix C *Calibration and Measurement Capabilities*



# Facility Components and design

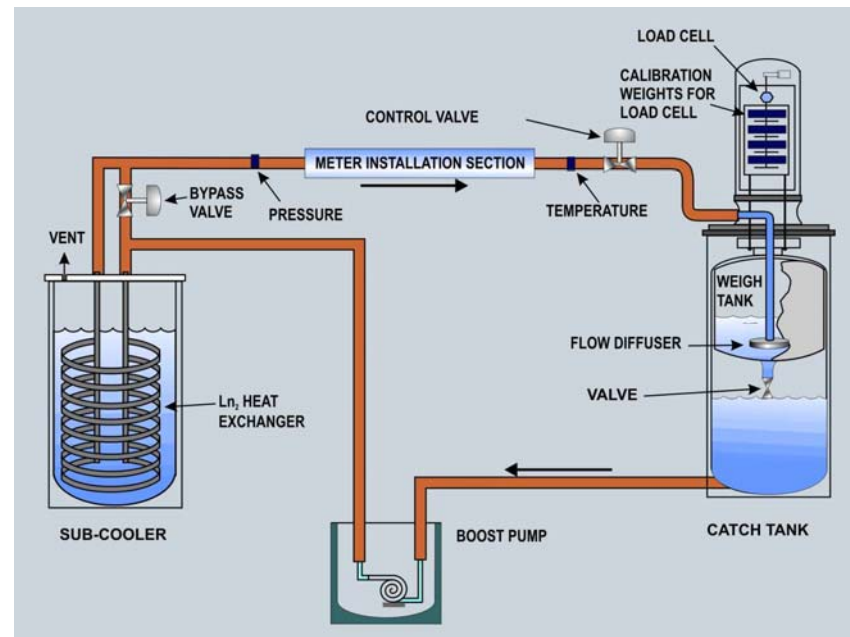
- Liquid nitrogen flow
  - Closed loop
- Mass Measurement
  - Load cell
  - Weigh tank
- Subcooler
  - Remove thermal energy
- Temperature measurement
  - PRT's
- Pressure measurement
  - Pressure transducer

# Liquid Nitrogen Flow Facility Schematic



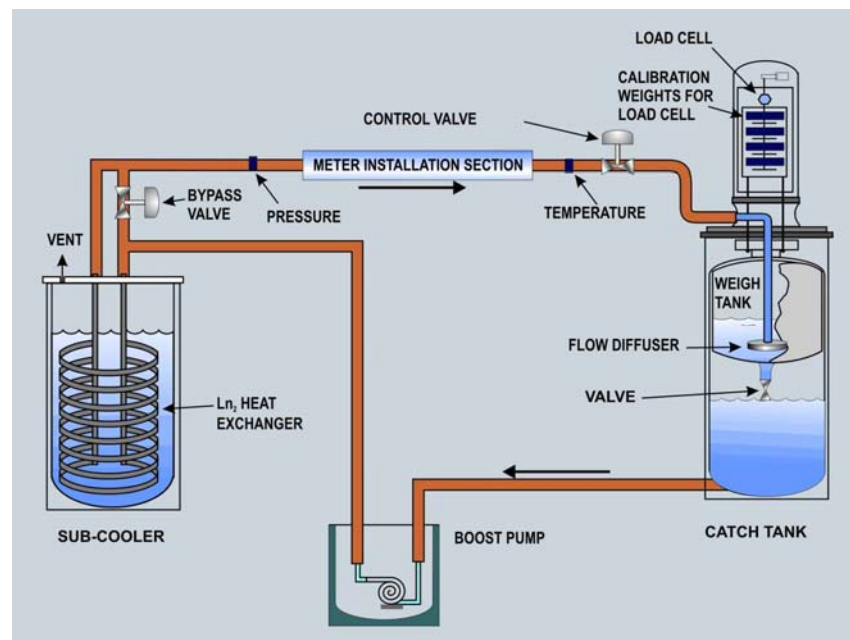
# Facility Description

- Liquid nitrogen is the process fluid
- Circulated throughout the closed loop by a variable speed pump
- Flows into a subcooler where thermal energy is removed
  - due to pumping
  - ambient heat leak
- Temperature in the test section controlled by
  - adjusting the subcooler liquid level
  - diverting flow around the subcooler
  - an inline heater
- Pressure in the test section controlled by
  - Downstream control valve
  - Introducing helium gas pressure



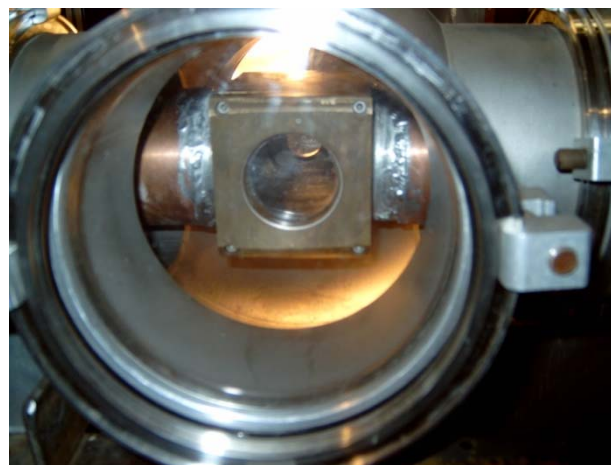
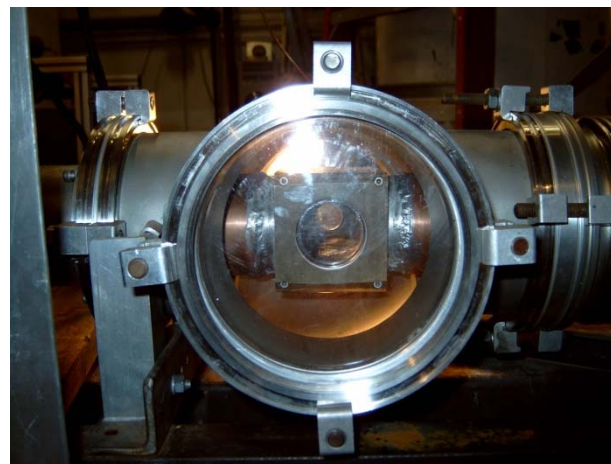
# Nitrogen Flow Procedure

- Catch tank liquid volume creates positive head pressure on centrifugal pump
  - Prevents cavitation and bubbling
- Fluid circulates in 76.2 mm vacuum-jacketed copper pipeline
- Liquid flows into diffuser to remove vertical component of velocity at bottom of aluminum weigh tank
  - 0.378 m<sup>3</sup> capacity
- Liquid flows through valve at bottom of weigh tank and into stainless steel pressure vessel
  - 0.443 m<sup>3</sup> capacity
- When temperature, pressure, and flowrate reach steady-state condition
  - weigh tank valve closed
  - System timers and data acquisition begin
  - Predetermined amount of liquid nitrogen accumulates in weigh tank
  - Varies from approx. 440 kg to 1320 kg
- Mass collected for each data point is determined by
  - Load cell output voltage values
  - Total time the mass was collected



# Liquid Nitrogen Flow Stream

- Sapphire window provides ability to observe flow directly downstream of flowmeter test section prior to entering weigh tank
- Internal liquid line is vacuum-jacketed to clearly view flow stream for gas bubbles



# Data Acquisition

- Once liquid level reaches preset value, test point begins
- Timer is initiated and data acquisition begins
- Frequency output from flowmeters is input into counters to totalize meter pulses
- Pressure and temperature are measured for density calculations in meter test section as well as in weigh and catch tanks for buoyancy calculations and system monitoring



# Uncertainty in Liquid Nitrogen Mass Flow Measurement

## Components of the mass flow uncertainty

- Load cell sensitivity measuring the mass of the LN2
  - Weights
  - Voltage
  - Sensitivity equation
  - Pressure
- Buoyancy evaluated for each mass measurement
  - Buoyancy of LN2 accumulated during the data point
  - Buoyancy of the immersed diffuser and pipe in LN2
  - Change in buoyancy of LN2 accumulated before the data point begins
- Time measurement
  - Multi-function datalogger used to measure within 1 ms
- Mass balance between test section and weigh tank
  - Finite volume of LN2 in piping between meter and weigh tank
  - Provided density gradient in pipe remains constant during data point, mass collected in weigh tank is equivalent to mass passing through meter
    - Pressure drop remains nearly constant
    - Temperature gradient less than 70 mK

## Total Uncertainties ( $1\sigma$ ) for Mass Measurement

Source of Uncertainty:	Type A (%)	Type B (%)	Combined (%)
Load Cell Sensitivity	0.050	0.002	.050
Buoyancy Correction	0.0001	0.068	0.068
Mass between Test Section and Weigh Tank (liquid N <sub>2</sub> )	0.011		
Total for Mass Measurement	0.051	0.068	0.085
Expanded Uncertainty, k=2			0.170
Time		0.001	0.001
Total for Mass Flow Rate	0.051	0.068	0.085
Expanded Uncertainty, k=2			0.170

# Total Uncertainties ( $1\sigma$ ) for Volumetric Flow Rate Measurement

Source of Uncertainty in Liquid Volume Flow	Nominal Values: T=85 K Mass = 182 kg P = 620 kPa Time = 100 s	
	Type A (%)	Type B (%)
EOS (REFPROP)		0.02
$\delta\rho/\delta T _P$	0.025	0.013
$\delta\rho/\delta P _T$ ( $P_{\text{Test Section, Baro}}$ )	0.0002	0.0002
Uncert. in mass flow rate	0.051	0.068
Total (in quad)	0.057	0.072
Total (Type A + B, in quad), k=2		0.184

# Calibration Procedure

- Statistical calibration program developed
  - Uses fractional factorial test plan
  - Provides ability to separate main effects and low-order interactions from one another
- Allows evaluation of meter for sensitivity to
  - Pressure
  - Temperature
  - Flowrate
  - Thermal cycling
- 60 data points taken over two-day period
  - 5 temperatures
  - 12 flowrates
  - 5 pressures

# Data Analysis

For volumetric flow rate, predicted performance of meter in measuring flow rate is compared to flow rate determined by facility:

Meter Mass: 
$$M_R = P\rho / K \quad (1)$$

Percent Deviation = 
$$(M_R - M_{NIST}) * 100 / M_{NIST} \quad (2)$$

Where,

- $M_R$  = mass calculated from the flowmeter output
- $P$  = flowmeter output in total pulses
- $\rho$  = liquid density determined from the flow facility temperature and pressure measurements
- $K$  = meter factor in pulses per unit volume
- $M_{NIST}$  = mass determined by the flow facility

For mass flow rate, only second equation is used

# Data Analysis

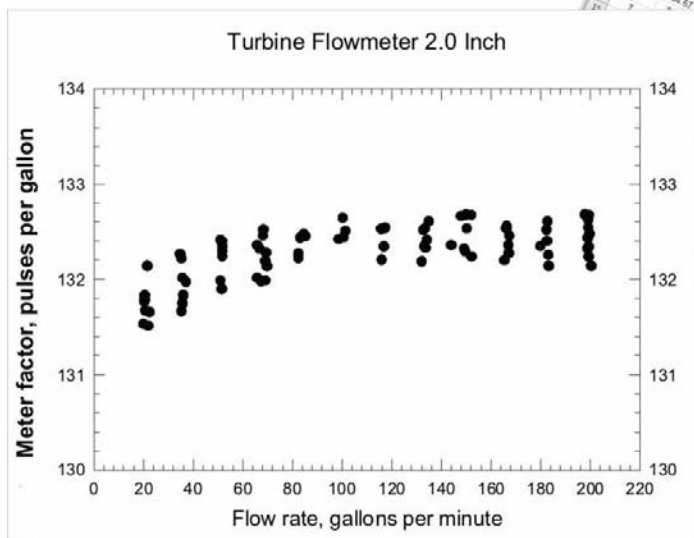
The deviation data are fitted by least-squares method to mathematical model equation:

$$\text{Dev}(\%) = A + BQ + CQ^2 + DQ^3 + ET + FP$$

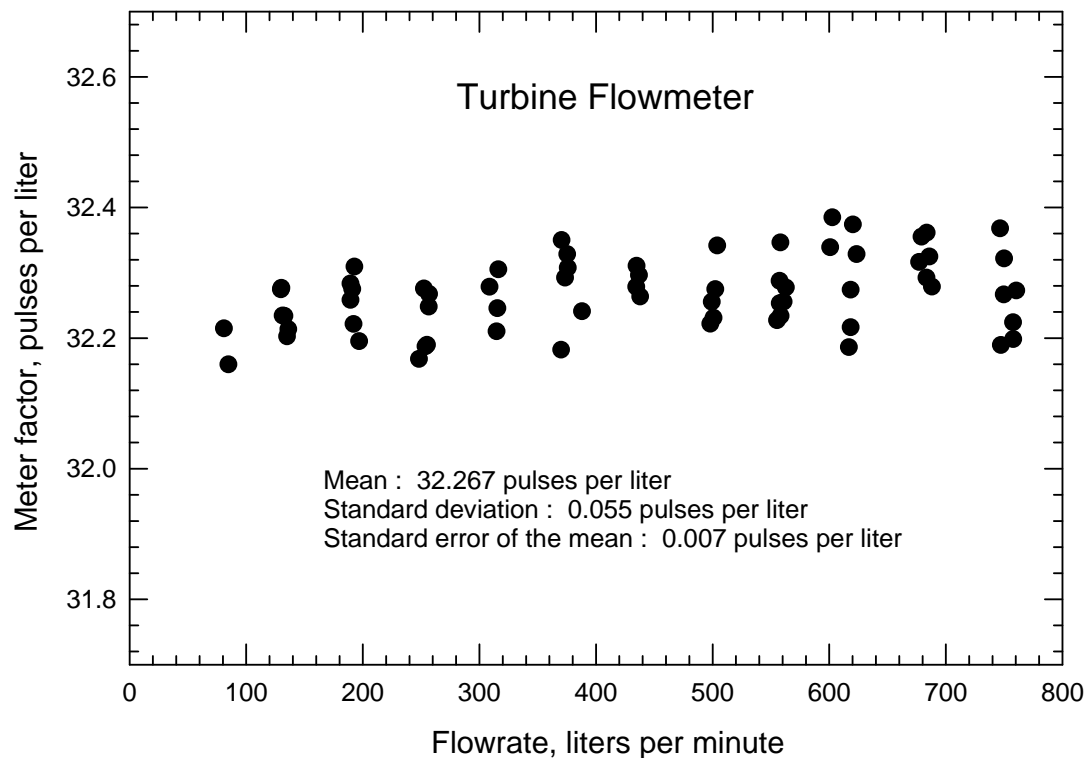
- Dev(%) = percent deviation
- T = fluid temperature
- Q = volume flowrate
- P = liquid nitrogen pressure
- A,B,C,D,E,F = coefficients



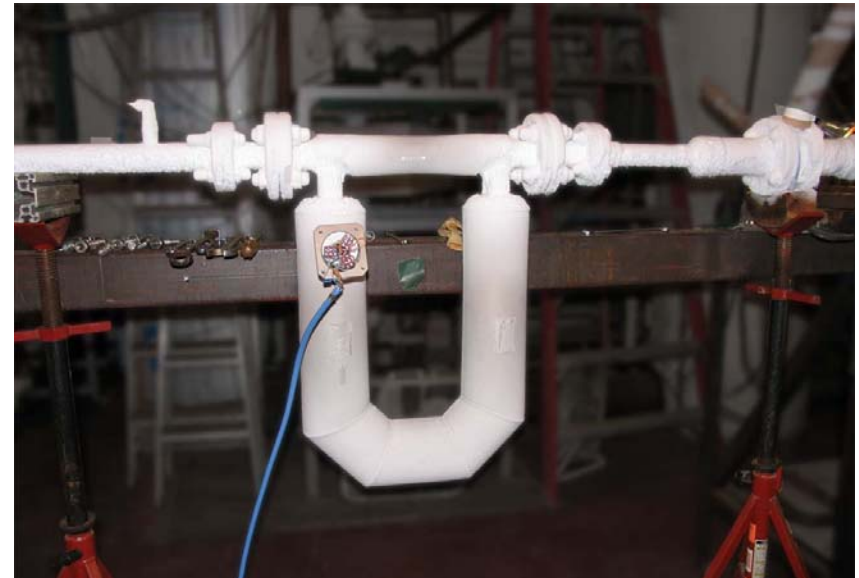
# Sample Data Results



# Typical Meter Calibration with Statistical Summary



# 38 mm Meter Installation

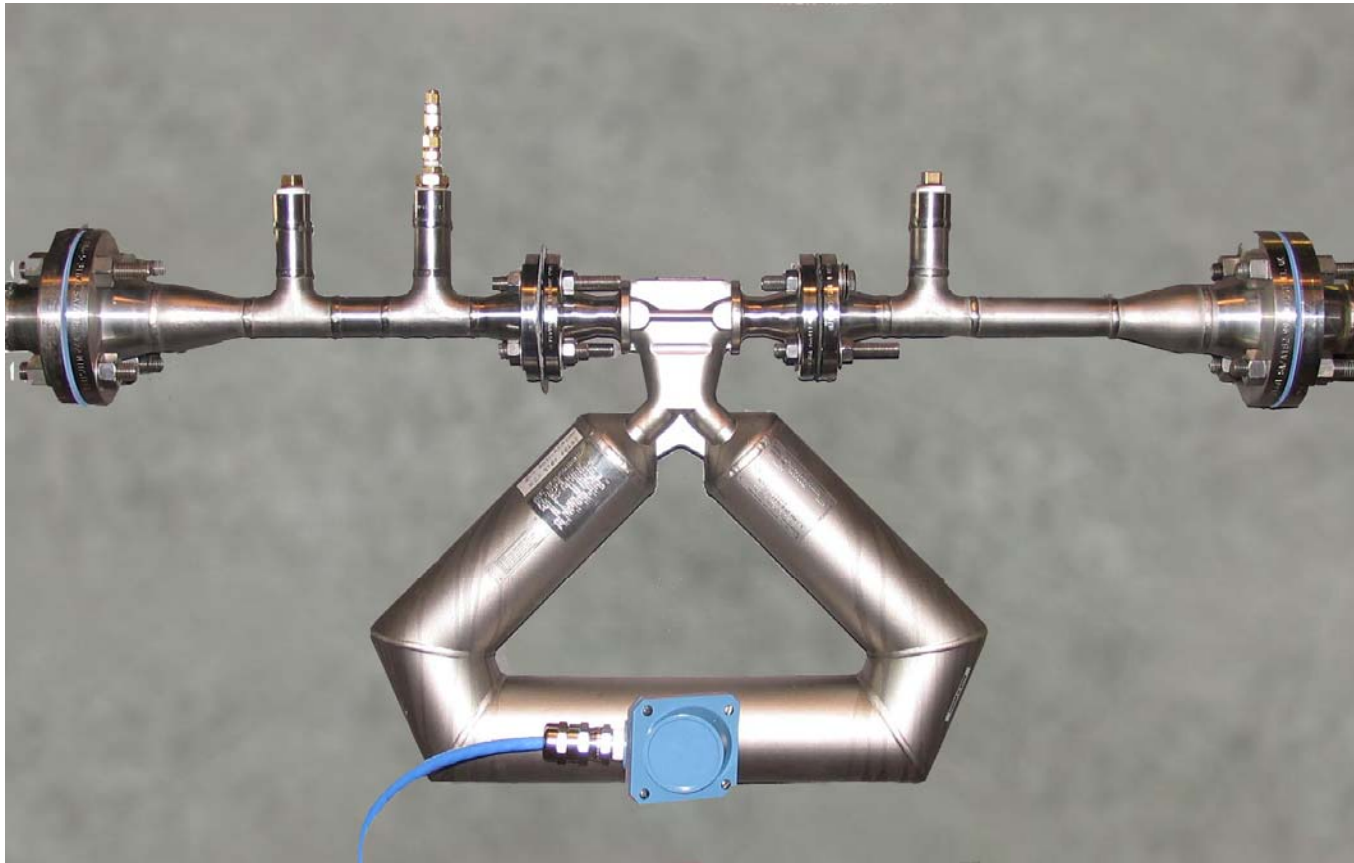


# 50 mm Flowmeter Installation





# 25 mm Flowmeter Installation



# 150 mm Flowmeter Installation





## Summary

- NIST Cryogenic Flow Facility is well instrumented in test section and weigh tank/catch tank assembly
- A meter evaluation test plan is used to determine sensitivity to pressure, temperature, flowrate, and thermal cycling
- Combined expanded uncertainties ( $k = 2$ ) for totalized mass and volume cryogenic flow measurement are 0.17% and 0.18% respectively
- Facility has been well used in evaluating various types of flowmetering devices to determine their suitability for measuring cryogenic flows
- It is anticipated that LNG and LH<sub>2</sub> will have expanding roles as alternative fuels, and NIST will be able to provide assistance in developing accurate measurement methods for cryogenic liquid flows

Thank you for your attention