

Example Table:

density = $f(\text{temperature } T, \text{ pressure } p, \text{ composition } x)$

TABLE 1

Experimental values of density ρ at temperature T , pressure p , and mole fraction x for the liquid mixtures ethanol(1) + linalool(2), propan-1-ol(1) + linalool(2), and propan-2-ol(1) + linalool(2).^a

T/K	p/MPa	x_1	$\rho/\text{kg}\cdot\text{m}^{-3}$	x_1	$\rho/\text{kg}\cdot\text{m}^{-3}$	x_1	$\rho/\text{kg}\cdot\text{m}^{-3}$
		ethanol(1) + linalool(2)		propan-1-ol(1) + linalool(2)		propan-2-ol(1) + linalool(2)	
283.15	0.100	0.0000	869.2	0.0000	869.5	0.0000	869.5
283.15	0.100	0.1129	866.8	0.1070	867.0	0.1031	866.3
283.15	0.100	0.8009	832.7	0.7985	835.9	0.7981	824.5
283.15	0.100	1.0000	797.7	1.0000	810.9	1.0000	793.7
283.15	5.000	0.0000	872.3	0.0000	872.6	0.0000	872.6
283.15	5.000	0.1129	869.9	0.1070	870.2	0.1031	869.5
283.15	5.000	0.8009	836.3	0.7985	839.3	0.7981	828.2
283.15	5.000	1.0000	801.8	1.0000	814.7	1.0000	797.5
283.15	10.000	0.0000	875.2	0.0000	875.7	0.0000	875.7
283.15	10.000	0.1129	872.9	0.1070	873.1	0.1031	872.5
283.15	10.000	0.3045	869.0	0.3066	868.3	0.3054	864.9
283.15	10.000	0.9009	825.5	0.8980	832.0	0.9092	816.6
283.15	10.000	1.0000	805.6	1.0000	818.1	1.0000	801.3
283.15	15.000	0.0000	878.2	0.0000	878.7	0.0000	878.7
283.15	15.000	0.4023	869.2	0.4064	868.3	0.4056	863.7
283.15	15.000	0.8009	843.1	0.7985	845.8	0.7981	835.1
283.15	15.000	1.0000	809.6	1.0000	821.7	1.0000	805.2
283.15	20.000	0.0000	881.0	0.0000	881.5	0.0000	881.5
283.15	20.000	0.1129	878.8	0.1070	879.0	0.1031	878.5
283.15	20.000	0.4023	872.1	0.4064	871.3	0.4056	866.7
283.15	20.000	0.9009	832.5	0.8980	838.6	0.9092	823.7
283.15	20.000	1.0000	813.1	1.0000	824.9	1.0000	808.9
298.15	0.100	0.0000	856.9	0.0000	857.3	0.0000	857.3
298.15	0.100	0.1129	854.5	0.1070	854.8	0.1031	854.1
298.15	0.100	0.5121	843.0	0.5010	843.2	0.5022	836.4
298.15	0.100	0.9009	805.9	0.8980	813.4	0.9092	796.8
298.15	0.100	1.0000	784.9	1.0000	799.0	1.0000	781.2
298.15	5.000	0.0000	860.1	0.0000	860.6	0.0000	860.6
298.15	5.000	0.1129	857.8	0.1070	858.1	0.1031	857.4
298.15	5.000	0.6055	841.4	0.6034	841.7	0.6050	833.3
298.15	5.000	0.7008	834.6	0.7055	835.1	0.7008	825.6
298.15	5.000	1.0000	789.3	1.0000	803.0	1.0000	785.5
298.15	10.000	0.0000	863.5	0.0000	863.9	0.0000	863.9
298.15	10.000	0.3045	857.2	0.3066	856.6	0.3054	853.2
298.15	10.000	0.5121	850.0	0.5010	850.1	0.5022	843.5
298.15	10.000	0.9009	813.9	0.8980	820.8	0.9092	804.9
298.15	10.000	1.0000	793.6	1.0000	806.9	1.0000	789.7
298.15	15.000	0.0000	866.6	0.0000	867.0	0.0000	867.0
298.15	15.000	0.1129	864.3	0.1070	864.6	0.1031	864.0
298.15	15.000	0.4023	857.7	0.4064	856.8	0.4056	852.0
298.15	15.000	0.6055	848.4	0.6034	848.5	0.6050	840.4
298.15	15.000	1.0000	797.7	1.0000	810.6	1.0000	793.8
298.15	20.000	0.0000	869.6	0.0000	870.0	0.0000	870.0
298.15	20.000	0.1129	867.4	0.1070	867.7	0.1031	867.0
298.15	20.000	0.4023	860.8	0.4064	859.9	0.4056	855.2
298.15	20.000	0.8009	835.1	0.7985	837.9	0.7981	826.9
298.15	20.000	1.0000	801.6	1.0000	814.1	1.0000	797.6

^a Standard uncertainties u are $u(T) = 0.01$ K, $u(p) = 0.016$ kPa for $p < 16$ MPa, $u(p) = 0.070$ kPa for $p > 16$ MPa, $u(x) = 0.0001$, and the combined expanded uncertainty U_c is $U_c(\rho) = 0.5$ $\text{kg}\cdot\text{m}^{-3}$ (0.95 level of confidence).